کنترل پیش بین Model Predictive Control

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Dynamic State Estimation for Dynamical Systems



- □ Introduce dynamic state estimation (DSE)
- Discuss classes of observers/estimators + Applications Briefly
- discuss stochastic estimators Kalman filter
- Deterministic observers
- □ State observer for MPC

Introduction

دانتگاهشی خارنسیرالدین علی

- □ What is dynamic state estimation (DSE)?
- -Accurately depicting what's happening inside a system
- Precisely: estimating internal system states
- -In circuits: voltages and currents
- -Water networks: amount of water flowing
- -Chemical plants: concentrations
- -Robots and UAVs: location & speed
- -Humans: temperature, blood pressure, glucose level
- □ So how does having estimates help me?
- -Well, if you have estimates, you can do control
- -And if you do good control, you become better off!
- □ In power systems: DSE can tell me what's happening to generators & lines⇒ Preventing/Predicting Blackouts!

Introduction



- **Dynamic observer:** dynamical system that observes the internal system state, given a set of input & output measurements
- **State estimator:** estimates the system's states under different assumptions Estimators: utilized for state estimation and parametric identification
- **Observers:** used for deterministic systems, Estimators: for stochastic dynamical systems
- □ If statistical information on process and measurement is available, stochastic estimators can be utilized
- □ This assumption is strict for many dynamical systems
- Quantifying distributions of measurement and process noise is very challenging

Stochastic estimators



- Stochastic estimators:
- -Extended Kalman Filter (EKF)
- -Unscented Kalman filter (UKF)
- -Square-root Unscented Kalman filter (SRUKF) -Cubature Kalman Filter (CKF)
- Stochastic estimators used if distributions of measurement & process noise are available

System dynamics:

$$x_{k} = f(x_{k-1}, u_{k-1}) + w_{k-1}$$

$$y_{k} = h(x_{k}, u_{k}) + v_{k}$$

$$-w_{k-1} \sim N(0, Q_{k-1}) \text{ and } v_{k} \sim N(0, R_{k}): \text{ process \& measurement noise}$$

$$-Q_{k-1} \text{ and } R_{k}: \text{ covariance of } q_{k-1} \& r_{k}$$

Stochastic Estimator: The Extended Kalman Filter



- Most stochastic estimators have two main steps: predictions & updates
- EKF (=KF+Nonlinearities) algorithm:
- (1) Prediction:

State esimate prediction: $\hat{x}_{k|k-1} = f(\hat{x}_{k-1|k-1}, u_{k-1})$ Predicted covariance estimate: $P_{k|k-1} = F_{k-1}P_{k-1|k-1}F_{k-1}^{\mathsf{T}} + Q_{k-1}$

(2) Update:

Innovation or measurement residual: Innovation (or residual) covariance: Near-optimal Kalman gain: Updated covariance estimate: Updated state estimate:

$$\begin{split} \tilde{\boldsymbol{y}}_k &= \boldsymbol{z}_k - h(\hat{\boldsymbol{x}}_{k|k-1}) \\ \boldsymbol{S}_k &= \boldsymbol{H}_k \boldsymbol{P}_{k|k-1} \boldsymbol{H}_k^\top + \boldsymbol{R}_k \\ \boldsymbol{K}_k &= \boldsymbol{P}_{k|k-1} \boldsymbol{H}_k^\top \boldsymbol{S}_k^{-1} \\ \boldsymbol{P}_{k|k} &= (\boldsymbol{I} - \boldsymbol{K}_k \boldsymbol{H}_k) \boldsymbol{P}_{k|k-1} \\ \hat{\boldsymbol{x}}_{k|k} &= \hat{\boldsymbol{x}}_{k|k-1} + \boldsymbol{K}_k \tilde{\boldsymbol{y}}_k \end{split}$$

$$\boldsymbol{F}_{k-1} = \left. \frac{\partial f}{\partial \boldsymbol{x}} \right|_{\hat{\boldsymbol{x}}_{k-1|k-1}, \boldsymbol{u}_{k-1}} , \ \boldsymbol{H}_{k} = \left. \frac{\partial h}{\partial \boldsymbol{x}} \right|_{\hat{\boldsymbol{x}}_{k|k-1}}$$

Determinstic Estimators (Observers)



- Deterministic observers for:
- –LTI systems
- -LTI systems + Unknown Inputs
- -LTI systems + Unknown Inputs + Measurement Noise
- -Nonlinear systems (bounded nonlinearity)
- -Nonlinear systems + Unknown Inputs
- -Nonlinear systems + Unknown Inputs + Measurement
- -LTI delayed systems
- -LTI delayed systems + Unknown Inputs
- -Hybrid systems
- -... and many more
- *Deterministic estimators used if measurement and process noise distributions are not available

Determinstic Estimators (Observers)



- Controllers often need values for the full state-vector of the plant
- This is nearly impossible in most complex systems
- Why?You simply can't put sensors everywhere, and some states are inaccessible
- **Observer:** a dynamical system that estimates the states of the system based on the plant's inputs and outputs
- Who introduced observers? David Luenberger in 1963, Ph.D. dissertation



LuenbergerObserver and Plant Dynamics



• Plant Dynamics:
$$\begin{cases} \dot{x} = Ax + Bu \\ y = Cx, \ x(0) \text{ not given} \end{cases}$$

Observers Dynamics:
$$\begin{cases} \dot{\hat{x}} = A\hat{x} + Bu + L(y - \hat{y}) \leftarrow Innovation \\ \dot{\hat{x}} = A\hat{x} + Bu + LC(x - \hat{x}) \end{cases}$$

• Error dynamics ²:

$$\dot{e} = \dot{x} - \dot{\hat{x}} = (A - LC)(x - \hat{x}) \rightarrow 0, \text{ as } t \rightarrow \infty, \text{ iff } \lambda_i(A - LC) < 0$$





Observer-Based Control

Closed-loop dynamics:

$$\dot{x} = Ax - BK\hat{x}$$

 $\dot{\hat{x}} = A\hat{x} + L(y - \hat{y}) - BK\hat{x}$

Or

$$\begin{bmatrix} \dot{x} \\ \dot{x} \end{bmatrix} = \begin{bmatrix} A & -BK \\ LC & A - LC - BK \end{bmatrix} \begin{bmatrix} x \\ \dot{x} \end{bmatrix}$$

• Transformation:
$$\begin{bmatrix} x \\ e \end{bmatrix} = \begin{bmatrix} x \\ x - \hat{x} \end{bmatrix} = \begin{bmatrix} I & 0 \\ I & -I \end{bmatrix} \begin{bmatrix} x \\ \dot{x} \end{bmatrix}$$

Hence, we can write:

$$\begin{bmatrix} \dot{x} \\ \dot{e} \end{bmatrix} = \underbrace{\begin{bmatrix} A - BK & BK \\ 0 & A - LC \end{bmatrix}}_{A_{\mathsf{cl}}} \begin{bmatrix} x \\ e \end{bmatrix}$$

- If the system is controllable & observable $\Rightarrow \texttt{eig}(A_{\mathsf{cl}})$ can be arbitrarily assigned by proper K and L
- What if the system is stabilizable and detectable?



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- Full state x(t) of process may not be available, only outputs y(t)
- Even if x(t) is available, noise should be filtered out
- Prediction and process models may be quite different
- The state x(t) may not have any physical meaning (e.g., in case of model reduction or subspace identification)

We need to use a state observer

• Example: Luenberger observer $\hat{x}(t+1) = A\hat{x}(t) + Bu(t) + L(y(t) - C\hat{x}(t))$



Note: the measurement noise model is not needed during optimization

Kalman filter design

Plant model

$$\begin{cases} x(t+1) = Ax(t) + B_u u(t) + B_v v(t) + B_d d(t) \\ y(t) = Cx(t) + D_v v(t) + D_d d(t) \end{cases}$$

• Full model for designing Kalman filter





Rudolf Emil Kalman (1930-2016)

$$\begin{bmatrix} x(t+1) \\ x_d(t+1) \\ x_m(t+1) \end{bmatrix} = \begin{bmatrix} AB_d \bar{C} & 0 \\ 0 & \bar{A} & 0 \\ 0 & 0 & \bar{A} \end{bmatrix} \begin{bmatrix} x(t) \\ x_d(t) \\ x_m(t) \end{bmatrix} + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} u(t) + \begin{bmatrix} B_v \\ 0 \\ 0 \end{bmatrix} v(t) + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} n_d(t) + \begin{bmatrix} 0 \\ 0 \\ \bar{B} \end{bmatrix} n_d(t) + \begin{bmatrix} 0 \\ 0 \\ \bar{B} \end{bmatrix} n_m(t) + \begin{bmatrix} B_u \\ 0 \\ 0 \end{bmatrix} n_u(t)$$
$$y_m(t) = \begin{bmatrix} C_m & D_{dm} \bar{C} & \bar{C} \end{bmatrix} \begin{bmatrix} x(t) \\ x_d(t) \\ x_m(t) \end{bmatrix} + D_{vm} v(k) + \bar{D}_m n_d(t) + \tilde{D}_m n_m(t)$$

- n_d(k) = source of modeling errors
- $n_m(k)$ = source of measurement noise
- $n_u(k)$ = white noise on input u (added to compute the Kalman gain)

I/O feedthrough



• We always assumed no feedthrough from u to measured \boldsymbol{y}

$$y_k = Cx_k + Du_k + D_v v_k + D_d d_k, \quad D_m = 0$$

- This avoids static loops between state observer, as $\hat{x}(t|t)$ depends on u(t) via $\hat{y}_m(t|t-1)$, and MPC (u(t) depends on $\hat{x}(t|t)$)
- Often D = 0 is not a limiting assumption as
 - often actuator dynamics must be considered (*u* is the set-point to a low-level controller of the actuators)
 - most physical models described by ordinary differential equations are strictly causal, and so is the discrete-time version of the model
- In case $D \neq 0$, we can assume a **delay** in executing the commanded u

$$y_k = C_m x_k + D u_{k-1}$$

and treat u(t-1) as an extra state

• Not an issue for **unmeasured** outputs

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